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## Welcome to CIPOA in Floripa!

On behalf of the Organizing and Scientific Committees, we extend a warm welcome to the 6th Iberoamerican Conference on Advanced Oxidation Technologies (VI CIPOA), taking place in Florianópolis, Brazil, from October 7th to 11th, 2024.

The CIPOA conference aims to bring together scientists, Ph.D. students, master's and undergraduate students, and professionals to share their research findings and engage in discussions about the future directions and opportunities in Advanced Oxidation Technologies. The focus areas encompass environmental protection, chemical and food engineering, energy, and climate sectors, all contributing to a sustainable and carbon-neutral circular economy.

The conference program will encompass a diverse range of engaging sessions, including invited lectures, oral communications, short oral communications for Ph.D. students, poster communications, and an interactive round-table discussion.

We cordially invite you to submit your abstracts for poster or oral presentations to the 6th Iberoamerican Conference on Advanced Oxidation Technologies. We eagerly await your contributions to the scientific program and sincerely appreciate your support in advance!

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### Organization



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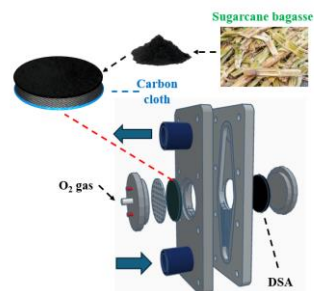
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This study investigates using sustainable sugarcane bagasse-based gas diffusion electrodes (GDEs) for H<sub>2</sub>O<sub>2</sub> generation and amoxicillin removal. While comparable H<sub>2</sub>O<sub>2</sub> production was achieved with traditional GDEs, sugarcane bagasse offered an eco-friendly alternative. The electrochemical advanced oxidation process (EAOP) combined (UVC-Fe-H<sub>2</sub>O<sub>2</sub>) effectively degraded amoxicillin (85% in 60 minutes) overcome methods like UVC or H<sub>2</sub>O<sub>2</sub> alone. Furthermore, the combined process demonstrated superior removal of total organic carbon (58.5%). Besides, the combination of EAOPs with electrogenerated H<sub>2</sub>O<sub>2</sub> and scalable electrochemical flow reactors (EFRs) offers a promising solution. Although, these findings suggest sugarcane bagasse GDEs with UVC-Fe-H<sub>2</sub>O<sub>2</sub> hold promise for treating antibiotic-contaminated water.

## Introduction

This work explores the use of gas diffusion electrodes (GDE) for a promising environmental application: generating hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) on-site to degrade pollutants. GDEs with carbon-based materials are highly efficient for H<sub>2</sub>O<sub>2</sub> production, but traditional options often rely on petroleum sources [1,2]. To address this, we present an sustainable alternatives like sugarcane bagasse, a readily available source of carbon. Additionally, the growing presence of antibiotics in the environment, particularly in water sources, necessitates effective treatment methods. Electrochemical advanced oxidation processes (EAOP) using electrogenerated H<sub>2</sub>O<sub>2</sub> offer a solution for eliminating these contaminants. Furthermore, the use of electrochemical flow reactors (EFR) enhances the scalability of this technology. Here we present an GDE based in sugarcane bagasse, applied in an flow reactor combined with EAOP (UVC-FE-H<sub>2</sub>O<sub>2</sub>), to remove commercial amoxicillin as a contaminant target.

## Material and Methods

### Chemicals

Commercially available amoxicillin pills were used. Ferrous sulfate heptahydrate (FeSO<sub>4</sub>·7H<sub>2</sub>O ≥ 99%, Vetec) served as the catalyst. Potassium sulfate (K<sub>2</sub>SO<sub>4</sub> 99%, Vetec) and sulfuric acid (H<sub>2</sub>SO<sub>4</sub> 95-98%, Vetec) were used for electrolyte preparation and pH adjustment. Ammonium molybdate ((NH<sub>4</sub>)<sub>6</sub>Mo<sub>7</sub>O<sub>24</sub>) solution (2.4×10<sup>-3</sup> mol L<sup>-1</sup>) was used for H<sub>2</sub>O<sub>2</sub> quantification. Acetonitrile (ACN, Sigma Aldrich) and ultrapure water from a Milli-Q® Direct-Q system (18.2 MΩ cm) (Merck Millipore) were used to prepare the mobile phases for liquid chromatography.

### Electrochemical setup

An electrochemical flow reactor (EFR) described elsewhere [3] was used to compare GDEs for H<sub>2</sub>O<sub>2</sub> generation. The setup had a 4 mm inter-electrode gap, 2.0 L capacity (semi-batch), and 10 L h<sup>-1</sup> flow rate controlled by a peristaltic pump. GDEs was fed with O<sub>2</sub> gas (99% purity) at 80 mL min<sup>-1</sup>. The 0.05 mol L<sup>-1</sup> electrolyte (pH 3.0) used a DSA®-Cl<sub>2</sub> anode (De Nora do Brazil) and either a commercial carbon GDE (CPL6) or a sugarcane bagasse GDE. Both electrodes had a 20 cm<sup>2</sup> exposed area.

### Experiments configurations

H<sub>2</sub>O<sub>2</sub> production of both GDEs (CPL6 and cane) was compared at various current densities (25-150 mA cm<sup>-2</sup>). Current efficiency (CE) and energy consumption (EC) were evaluated using equations **eq. 1** and **eq. 2** for a more comprehensive comparison.

$$CE(\%) = \frac{2F c_1 V}{I t_1} \times 100 \quad (\text{eq. 1})$$

$$EC(\text{kWh kg}^{-1}) = \frac{1000 E I t_2}{M} \quad (\text{eq. 2})$$

The terms in both equations can be find in this work [3]. The EAOP tests for degradation of 20 mg L<sup>-1</sup> amoxilin was performed in the same electrochemical conditions describe before. The UV-C light used was low-pressure Hg lamp (254 nm; Philips). For Fenton reactions 2.5 μmol L<sup>-1</sup> of FeSO<sub>4</sub> was used. Also blank experiments to better evaluation of effect of each EAOP process is performed.

### Gas diffusion electrode preparation

We built the electrode following our prior method [3]. Briefly, we mixed 80% carbon mass with 20% PTFE and pressed it onto a ZOLTEK carbon cloth

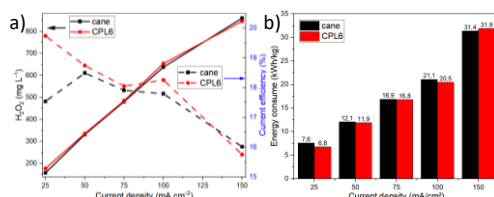
at 4.5 tons, 290°C for 15 minutes.

### Analytical method

Amoxicillin was measured using an HPLC system (Shimadzu, series 20) with a DAD, employing a C18 column and 50% ACN: 50% H<sub>2</sub>O U.P. as the mobile phase at a flow rate of 1.0 mL min<sup>-1</sup>. The mineralization extent was monitored by total organic carbon (TOC) determination using a Shimadzu TOC-VCPN. H<sub>2</sub>O<sub>2</sub> was measured at intervals during the 1-hour experiment. Samples were mixed with ammonium molybdate, forming a detectable compound at 350 nm for analysis [4]. Subsequently, UV-1900 spectrophotometer (Shimadzu) was used for analysis.

### Results and Discussion

In Figure 1-a is shown the current densities tests and de concentration of H<sub>2</sub>O<sub>2</sub>, for both GDEs (CPL6 and cane), after 60 min of electrolysis.



**Figure 1.** Comparison between GDEs (CPL6 and cane), by varying current densities **a)** Concentration of H<sub>2</sub>O<sub>2</sub> and current efficiency, **b)** Energy consumption.

For all current densities applied (25 to 150 mA cm<sup>-2</sup>), the concentration of H<sub>2</sub>O<sub>2</sub> electrogenerated is almost the same for both GDEs. However, for the lowest current density applied (25 mA cm<sup>-2</sup>), the efficiency was the most different (17.5 and 19.7 %, for cane and CPL6, respectively). Although, the analysis of energy consumption (Figure 1-b) show less than 1 kWh kg<sup>-1</sup> difference between both GDEs, for all current densities.

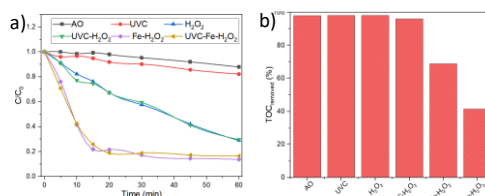
The degradation of commercial amoxicillin (Amox) in different EAOPs (anodic oxidation (AO), ultraviolet in 254 nm (UVC), H<sub>2</sub>O<sub>2</sub> electrogenerated (H<sub>2</sub>O<sub>2</sub>) and Fenton combination with H<sub>2</sub>O<sub>2</sub> and UVC (Fe-H<sub>2</sub>O<sub>2</sub> and UVC-Fe-H<sub>2</sub>O<sub>2</sub>)) conditions is presented in Figure 2.

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**Figure 2.** Use of GDE of cane in different EAOP condition applied in Amox degradation, **a)** degradation curve, **b)** TOC removed. Electrochemical condition: 25 mA cm<sup>-2</sup>, pH 3, 2.0 L at 0.05 mol L<sup>-1</sup> of K<sub>2</sub>SO<sub>4</sub> solution, and 20 mg L<sup>-1</sup> of amoxicillin.

Figure 2-a shows the degradation curves for amoxicillin removal. Conditions with only AO (anodic oxidation) and UVC (ultraviolet C radiation) have low effectiveness, reaching only 12.0% and 18.0% removal after 60 minutes, respectively. Similarly, the removal of total organic carbon (TOC) for both conditions is close to zero (Figure 2-b). Electrogenerated hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) and its combination with UVC show a better, and practically identical, effect on amoxicillin degradation, removing around 30.0% after 60 minutes. However, the H<sub>2</sub>O<sub>2</sub> condition alone removes almost no TOC, while UVC-H<sub>2</sub>O<sub>2</sub> removes only 4.0%. The best response for amoxicillin degradation is found for the electro-Fenton reaction (Fe-H<sub>2</sub>O<sub>2</sub>) and its combination with UVC (UVC-Fe-H<sub>2</sub>O<sub>2</sub>). Both conditions also exhibit very similar degradation curves, reaching 80.0% removal after 15 minutes of reaction, with a slight decrease to 85.0% at 60 minutes (Figure 2-a). However, for TOC removal, the combined process (UVC-Fe-H<sub>2</sub>O<sub>2</sub>) shows a better effect (58.5%) compared to the electro-Fenton process alone (31.1%).

### Conclusions

The results show that GDE made with sugarcane bagasse have practically the same efficiency of the well-know commercial carbon printex L6. Also, in application of EAOP process, the combination of UVC-Fe-H<sub>2</sub>O<sub>2</sub>, show the most effective method for amoxicillin removal from water. It achieved a remarkable 85% degradation, and 58.5% of TOC removed within just 60 minutes, significantly outperforming alternative methods like AO, UVC, and even H<sub>2</sub>O<sub>2</sub> alone.